

**BIRLA INSTITUTE OF TECHNOLOGY, MESRA, RANCHI
(END SEMESTER EXAMINATION)**

**CLASS: M.Sc
BRANCH: Biotechnology**

**SEMESTER : II
SESSION : SP/2024**

SUBJECT: BT416 ENZYME & BIOPROCESS TECHNOLOGY

TIME: 3 Hours

FULL MARKS: 50

INSTRUCTIONS:

1. The question paper contains 5 questions each of 10 marks and total 50 marks.
2. Attempt all questions.
3. The missing data, if any, may be assumed suitably.
4. Before attempting the question paper, be sure that you have got the correct question paper.
5. Tables/Data hand book/Graph paper etc. to be supplied to the candidates in the examination hall.

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|---|------|------|------|----------------------------------|------|------|------|------|------|----------------------|----|----|----|-----|----|------------|---|---|---|---|---|----|----|----|----|----|----|--------------|----|----|-----|-----|----|----|----|----|----|----|----|
| Q.1(a) Justify that 'biomass produced in a turbidostat is a function of limiting substrate used and yield of biomass on it'. | [5] | 1 | 5 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.1(b) Discuss the application of Luedeking- Piret equation for product formation. Modify Luedeking- Piret equation for growth associated and non- growth associated product formation. | [5] | 1 | 5 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.2(a) Glucose oxidase was allowed for catalysis in the presence of glucose. The following data were obtained. Calculate V_{max} and K_m . Given $[E_o] = 0.02$ g/l. | [5] | 2 | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <table border="1" style="width: 100%; border-collapse: collapse; text-align: center;"> <tr> <td style="width: 15%;">V_o (g/l-min)</td> <td style="width: 15%;">0.88</td> <td style="width: 15%;">0.77</td> <td style="width: 15%;">0.58</td> <td style="width: 15%;">0.42</td> <td style="width: 15%;">0.25</td> </tr> <tr> <td>S_o (g/l)</td> <td>60</td> <td>38</td> <td>20</td> <td>8.0</td> <td>3</td> </tr> </table> | | | | V _o (g/l-min) | 0.88 | 0.77 | 0.58 | 0.42 | 0.25 | S _o (g/l) | 60 | 38 | 20 | 8.0 | 3 | | | | | | | | | | | | | | | | | | | | | | | | |
| V _o (g/l-min) | 0.88 | 0.77 | 0.58 | 0.42 | 0.25 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| S _o (g/l) | 60 | 38 | 20 | 8.0 | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.2(b) Propose methods for immobilization of enzyme by adsorption and ionic bonding. Compare two techniques. | [5] | 2 | 6 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.3(a) What do mean by sterilization of medium in fermentation industry? Derive an expression to show the death kinetics in batch autoclave. | [5] | 3 | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.3(b) Draw a bioreactor and illustrate the aeration system present in it. Also, explain how to achieve aseptic aeration in bioreactor. | [5] | 3 | 4 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.4(a) Draw a bioreactor and illustrate the agitation system present in it. Also, explain processes of mixing and aseptic operation in it. | [5] | 2 | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.4(b) Calculate the K_{La} value from the given data of bacterial culture (3 g/L) in a CSTR. Given that $C^* = 7.8$ mg/L. | [5] | 2 | 3 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| <table border="1" style="width: 100%; border-collapse: collapse; text-align: center;"> <tr> <td style="width: 15%;">DO (% O₂ saturation)</td> <td style="width: 10%;">48</td> <td style="width: 10%;">48</td> <td style="width: 10%;">48</td> <td style="width: 10%;">21</td> <td style="width: 10%;">7</td> <td style="width: 10%;">11</td> <td style="width: 10%;">18</td> <td style="width: 10%;">32</td> <td style="width: 10%;">37</td> <td style="width: 10%;">42</td> <td style="width: 10%;">45</td> </tr> <tr> <td>Time (min)</td> <td>0</td> <td>2</td> <td>4</td> <td>6</td> <td>8</td> <td>10</td> <td>12</td> <td>14</td> <td>16</td> <td>18</td> <td>20</td> </tr> <tr> <td>Air (on/off)</td> <td>on</td> <td>on</td> <td>off</td> <td>Off</td> <td>on</td> <td>on</td> <td>on</td> <td>on</td> <td>on</td> <td>on</td> <td>on</td> </tr> </table> | | | | DO (% O ₂ saturation) | 48 | 48 | 48 | 21 | 7 | 11 | 18 | 32 | 37 | 42 | 45 | Time (min) | 0 | 2 | 4 | 6 | 8 | 10 | 12 | 14 | 16 | 18 | 20 | Air (on/off) | on | on | off | Off | on | on | on | on | on | on | on |
| DO (% O ₂ saturation) | 48 | 48 | 48 | 21 | 7 | 11 | 18 | 32 | 37 | 42 | 45 | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Time (min) | 0 | 2 | 4 | 6 | 8 | 10 | 12 | 14 | 16 | 18 | 20 | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Air (on/off) | on | on | off | Off | on | on | on | on | on | on | on | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.5(a) Draw the steps you will undertake to design a bioreactor of 50000L for production of metabolite A from bacteria B on medium C. It may be supposed that initial data is available from 5 L laboratory bioreactor. | [5] | 3 | 6 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |
| Q.5(b) Justify the statement that 'for primary metabolite production in CSTR, continuous culture is better'. | [5] | 3 | 6 | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | | |

:26/04/2024 E: