

**BIRLA INSTITUTE OF TECHNOLOGY, MESRA, RANCHI
(END SEMESTER EXAMINATION)**

CLASS: IMSC
BRANCH: FOOD TECHNOLOGY

SEMESTER : VI
SESSION : SP/2023

SUBJECT: FT309 MASS TRANSFER IN FOOD PROCESSING

TIME: 3 Hours

FULL MARKS: 50

INSTRUCTIONS:

1. The question paper contains 5 questions each of 10 marks and total 50 marks.
2. Attempt all questions.
3. The missing data, if any, may be assumed suitably.
4. Before attempting the question paper, be sure that you have got the correct question paper.
5. Graph paper to be supplied to the candidates in the examination hall.

- | | [5] | CO | BL | | | | | | | | | | | | | | | | | | |
|--|--------|--------|--------|-------|-------|-------|-------|-------|------|---|--------|--------|-------|-------|-------|-------|-------|-------|--|--|--|
| Q.1(a) A sphere of naphthalene having a radius of 2.0mm is suspended in a large volume of still air at 318k and $1.01325 \times 10^5 \text{ Pa}$ (1atm). The surface temperature of the naphthalene can be assumed to be at 318K and its vapour pressure at 318K is 0.555mm of Hg. The D_{AB} of naphthalene in air at 318K is $6.92 \times 10^{-6} \text{ m}^2/\text{Sec}$. Calculate the rate of evaporation of naphthalene from surface. | [5] | CO-1 | 3 | | | | | | | | | | | | | | | | | | |
| Q.1(b) Calculate the rate of diffusion of hydrogen (A) through nondiffusing methane (B) at 25°C and 101 kN/m^2 pressure ($D_{AB} = 6.6 \times 10^{-5} \text{ m}^2/\text{s}$). The diffusion path is 5 mm long and the concentration of hydrogen at the two ends of the path in terms of partial pressure is 12 kN/m^2 and 8.4 kN/m^2 respectively.) | [5] | CO-1 | 3 | | | | | | | | | | | | | | | | | | |
| Q.2(a) A continuous fractionating column operating at atmospheric pressure is to separate a feed containing 30% CS_2 and 70% CCl_4 into an overhead product of 95 % CS_2 and a bottom product of 95 mole % CCl_4 . The feed enters as a saturated liquid at its boiling point. Assuming an overall plate efficiency of 70% and a reflux ratio is 1.5. Estimate the number of plates needed. All the compositions are in mole %.
Equilibrium data: | [5] | CO-2 | 3 | | | | | | | | | | | | | | | | | | |
| <table border="1" style="margin-left: auto; margin-right: auto; border-collapse: collapse;"> <tbody> <tr> <td style="padding: 5px;">x</td> <td style="padding: 5px;">0.0296</td> <td style="padding: 5px;">0.0615</td> <td style="padding: 5px;">0.258</td> <td style="padding: 5px;">0.39</td> <td style="padding: 5px;">0.532</td> <td style="padding: 5px;">0.663</td> <td style="padding: 5px;">0.758</td> <td style="padding: 5px;">0.86</td> </tr> <tr> <td style="padding: 5px;">y</td> <td style="padding: 5px;">0.0823</td> <td style="padding: 5px;">0.1555</td> <td style="padding: 5px;">0.494</td> <td style="padding: 5px;">0.634</td> <td style="padding: 5px;">0.747</td> <td style="padding: 5px;">0.830</td> <td style="padding: 5px;">0.880</td> <td style="padding: 5px;">0.932</td> </tr> </tbody> </table> | x | 0.0296 | 0.0615 | 0.258 | 0.39 | 0.532 | 0.663 | 0.758 | 0.86 | y | 0.0823 | 0.1555 | 0.494 | 0.634 | 0.747 | 0.830 | 0.880 | 0.932 | | | |
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| y | 0.0823 | 0.1555 | 0.494 | 0.634 | 0.747 | 0.830 | 0.880 | 0.932 | | | | | | | | | | | | | |
| Q.2(b) Discuss application of azeotropic and steam distillation. Give Flow sheet to explain the processes. | [5] | CO-2 | 2 | | | | | | | | | | | | | | | | | | |
| Q.3(a) Discuss the factors which govern the selection of solvents to be used for liquid-liquid extractions. What is Extract and Raffinate. | [5] | CO-3 | 2 | | | | | | | | | | | | | | | | | | |
| Q.3(b) The temperature of air in a room is 26.7°C and the total pressure is 101.3 kPa abs. The air contains water vapor with a partial pressure $P_A = 2.76 \text{ kPa}$. [vapor pressure of water, $P_{AS} = 3.5 \text{ kPa}$] Calculate
(i) the humidity
(ii) the saturation humidity and percentage humidity
(iii) the percentage relative humidity | [5] | CO-5 | 3 | | | | | | | | | | | | | | | | | | |
| Q.4(a) Derive expression Langmuir adsorption isotherm with assumption. | [5] | CO-4 | 3 | | | | | | | | | | | | | | | | | | |
| Q.4(b) A solute of $\text{K}_2\text{Cr}_2\text{O}_7$ in water contains 15% by wt $\text{K}_2\text{Cr}_2\text{O}_7$. Determine the amount of $\text{K}_2\text{Cr}_2\text{O}_7$ that can be produced from 1500 Kg of solution if 700 Kg of water is evaporated and remaining solution is cooled to 20°C . The solubility of $\text{K}_2\text{Cr}_2\text{O}_7$ at 20°C is 115 Kg/1000 Kg of water. | [5] | CO-4 | 3 | | | | | | | | | | | | | | | | | | |
| Q.5(a) Define:
(i) Bound moisture (ii) Equilibrium moisture (iii) Typical drying rate curve and bring out its salient features. | [5] | CO-5 | 2 | | | | | | | | | | | | | | | | | | |
| Q.5(b) A time of 5 hr was taken to dry a material from an initial moisture of 30% to a final moisture of 7%. Critical and equilibrium moisture are found to be 15% and 2% respectively. How much further time would be required to dry the material to final moisture of 4%. All moisture contents are on wet basis. | [5] | CO-5 | 3 | | | | | | | | | | | | | | | | | | |