BIRLA INSTITUTE OF TECHNOLOGY, MESRA, RANCHI (MID SEMESTER EXAMINATION)

CLASS: BE BRANCH: CHEMICAL ENGG.

SUBJECT : CL6009 ADVANCES IN REACTION ENGINEERING

TIME: 1.5 HOURS FULL MARKS: 25 INSTRUCTIONS: 1. The total marks of the questions are 30. 2. Candidates may attempt for all 30 marks. 3. In those cases where the marks obtained exceed 25 marks, the excess will be ignored. 4. Before attempting the question paper, be sure that you have got the correct question paper. 5. The missing data, if any, may be assumed suitably. _____ Q1 Discuss the non-isothermal multiple chemical reactions in PFR and CSTR reactors. [5] Q2 Parallel reaction in a PFR with heat effects: [5] The following gas-phase reactions occur in a PFR: $A \xrightarrow{k_1} B -r_{1A} = k_{1A}C_A$ Reaction 1: $2A \xrightarrow{k_1} C \quad -r_{2A} = k_{2A}C_A^2$ Reaction 2: Pure A is fed at a rate of 100 mol/s, a temperature of 150°C and a concentration of 0.1 mol/dm³. Determine the temperature and flow rate profiles down the reactor. Additional information: $\Delta H_{R_{ALA}} = -20,000 \text{ J/(mol of A reacted in reaction 1)}$ $\Delta H_{R_{X2A}} = -60,000 \text{ J/(mol of A reacted in reaction 2)}$ $C_{P_{A}} = 90 \text{ J/mol} \cdot {}^{\circ}\text{C}$ $k_{1A} = 10 \exp\left[\frac{E_{1}}{R}\left(\frac{1}{300} - \frac{1}{T}\right)\right] \text{s}^{-1}$ $C_{P_{\rm B}} = 90 \text{ J/mol}^{\circ}\text{C}$ $E_1/R = 4000 \text{ K}$ $C_{P_{\rm C}} = 180 \text{ J/mol}^{\circ}\text{C}$ $k_{2\rm A} = 0.09 \exp\left[\frac{E_2}{R}\left(\frac{1}{300} - \frac{1}{T}\right)\right] \frac{\mathrm{d}m^3}{\mathrm{mol}^{\circ}\mathrm{s}}$ $Ua = 4000 \, \text{J/m}^3 \cdot \text{s} \cdot \text{°C}$ $E_{\gamma}/R = 9000 \text{ K}$

- $T_{a} = 100^{\circ} C$
- Q3 Discuses and derive the expression for Langmuir adsorption isotherm.
- Q4 A solid catalyst is prepared by using the alumina particles (100 to 150 mesh size). This [5] catalyst is then made into large cylindrical pellets for rate studies. The Al₂0₃ particles contain micropores, and the pelletting process introduces macropores surrounding the particles. From the experimental methods, the macropore volume of one pellet is 0.645 cm³ and the micropore volume is 0.40 cm³/g of particles. The gross measurements for

one pellet are Mass = 3.15 g; Diameter = 1.00 in.; Thickness = 1/4 in.; Volume = 3.22 cm³ From this information calculate:

- (a) The micropore void fraction in the pellet
- (b) The solid fraction
- (c) The-density of the particles
- (d) The density of the solid phase
- (e) The void fraction of the particles

[5]

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- Q5 Describe the Shrinking-Core model for spherical particles of unchanging size with the [5] help of a clear sketch.
- Q6 Hydrogen sulfide is absorbed by a solution of methanolamine (MEA) in a packed column. [5] At the top of the column, gas is at 20 atm and it contains 0.1% of H₂S, while the absorbent contains 250 mol/m³ of free MEA. The diffusivity of MEA in solution is 0.64 times that of H₂S. The reaction is normally regarded as irreversible and instantaneous.

$$\frac{H_2S + RNH_2 \rightarrow HS^- + RNH_3}{(A)}$$

For the flow rates and packing used $k_{\rm Al}a=0.03~{
m s}^{-1}$

 $k_{Ag}a = 60 \text{ mol/m}^3 \cdot \mathbf{s} \cdot \mathbf{atm}$

 $H_{\rm A} = 1 \times 10^{-4} \, {\rm m^3 \cdot atm/mol}$, Henry's law constant for H₂S in water.

(a) Find the rate of absorption of H_2S in MEA solution.

(b) To find out whether it is worthwhile using MEA absorbent, determine how much faster is absorption with MEA compared to absorption in pure water.



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