

**BIRLA INSTITUTE OF TECHNOLOGY, MESRA, RANCHI
(END SEMESTER EXAMINATION)**

CLASS : BTECH
BRANCH: CHEMICAL ENGG/FOOD TECH
SUBJECT: CL24207 HEAT TRANSFER OPERATIONS

SEMESTER : III
SESSION : MO/2025

TIME: 3 Hours

FULL MARKS: 50

INSTRUCTIONS:

1. The question paper contains 5 questions each of 10 marks and total 50 marks.
2. Attempt all questions.
3. The missing data, if any, may be assumed suitably.
4. Before attempting the question paper, be sure that you have got the correct question paper.
5. Tables/Data hand book/Graph paper etc. to be supplied to the candidates in the examination hall.

		CO	BL
Q.1(a) A furnace wall is made of three layers – firebrick (0.10 m, $k = 1.4 \text{ W/m}\cdot\text{K}$), insulation brick (0.08 m, $k = 0.2 \text{ W/m}\cdot\text{K}$), and steel plate (0.01 m, $k = 45 \text{ W/m}\cdot\text{K}$). The inner surface temperature is 900°C and the outer surface temperature is 120°C . Find: (a) The rate of heat loss per m^2 of wall, and (b) The temperature at the interface between the insulation brick and steel layer.	[5]	1	3
Q.1(b) An aluminum cube ($k = 240 \text{ W/m}\cdot\text{K}$, $\rho = 2700 \text{ kg/m}^3$, $c_p = 900 \text{ J/kg}\cdot\text{K}$) with side length 3 cm is initially at 350°C . It is placed in a fluid at 50°C with $h = 120 \text{ W/m}^2\cdot\text{K}$. a) Calculate the time constant of the cube. b) What is the temperature of the cube after 45 seconds? c) What is the initial rate of cooling of the cube (in $^\circ\text{C/s}$)?	[5]	1	3
Q.2(a) Discuss how the thickness of the thermal boundary layer varies with: (i) Reynolds number (ii) Prandtl number Schematically show the velocity and thermal boundary layer profiles on a heated flat plate.	[5]	2	2
Q.2(b) Water at 25°C enters a copper tube ($D = 25 \text{ mm}$, $L = 2 \text{ m}$) with a velocity of 1.5 m/s . The wall temperature is constant at 80°C . Properties at mean temperature: $\rho = 997 \text{ kg/m}^3$, $\mu = 0.001 \text{ Pa}\cdot\text{s}$, $c_p = 4180 \text{ J/kg}\cdot\text{K}$, $k = 0.6 \text{ W/m}\cdot\text{K}$, $Pr = 5.0$ Calculate: (a) The average heat transfer coefficient, and (b) The heat transfer rate. (Use Dittus-Boelter equation)	[5]	2	3
Q.3(a) Describe Wein's Displacement law and Stefan-Boltzmann's law.	[5]	3	2
Q.3(b) Discuss the concept of radiation shields and outline their practical applications.	[2]	3	2
Q.3(c) A thin aluminium sheet with an emissivity of 0.1 on both sides is placed between two very large parallel plates that are maintained at uniform temperatures $T_1 = 800 \text{ K}$ and $T_2 = 500 \text{ K}$ and have emissivities $\epsilon_1 = 0.2$ and $\epsilon_2 = 0.7$. Determine the net rate of radiation heat transfer between the two plates per unit surface area of the plates and compare the result to that without the shield.	[3]	3	3
Q.4(a) Define: steam economy, boiling point elevation, film boiling, nucleate boiling.	[5]	4	2
Q.4(b) Draw a schematic of a triple-effect forward-feed evaporator and write the corresponding material balance and energy balance equations for each effect with assumptions.	[5]	4	3
Q.5(a) Describe the construction and working of a floating head shell-and-tube heat exchanger. Discuss its main components, advantages, and disadvantages.	[5]	5	2
Q.5(b) A shell-and-tube heat exchanger employs a liquid in the shell that is heated from 30°C to 55°C by a hot gas in the tubes that is cooled from 100°C to 60°C . Calculate the effectiveness of the heat exchanger.	[2]	5	3
Q.5(c) A small steam condenser is designed to condense 0.76 kg/min of steam at 83 kPa with cooling water at 10°C . The exit temperature is not to exceed 57°C . The overall heat-transfer coefficient is $3400 \text{ W/m}^2\cdot^\circ\text{C}$. Calculate the area required for a double-pipe heat exchanger. $T_{\text{sat}} = 95.6^\circ\text{C}$, $h_{\text{fg}} = 2.27 \times 10^6 \text{ J/kg}$.	[3]	5	3